

## Appendix I

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### Rheological Properties of biscuit dough

Temperature dependence: polynomial fitting of  $s$  from oscillatory data

$$s(T) = \exp\left(A_{Esse} + B_{Esse} \cdot T + C_{Esse} \cdot T^2 + D_{Esse} \cdot T^3 + E_{Esse} \cdot T^4 + F_{Esse} \cdot T^5\right)$$

$$A_{Esse} = 39.10635203$$

$$B_{Esse} = -2.29384768$$

$$C_{Esse} = 0.070502236$$

$$D_{Esse} = -0.001074$$

$$E_{Esse} = 0.00000808715$$

$$F_{Esse} = -0.000000023735$$

Temperature dependence: polynomial fitting of  $\alpha$  from oscillatory data

$$\alpha = \exp\left(A_{Alfa} + B_{Alfa} \cdot T + C_{Alfa} \cdot T^2 + D_{Alfa} \cdot T^3 + E_{Alfa} \cdot T^4\right)$$

$$A_{Alfa} = -2.868703$$

$$B_{Alfa} = 0.104545$$

$$C_{Alfa} = -0.001971$$

$$D_{Alfa} = 0.0000127$$

$$E_{Alfa} = -0.0000000262$$

### Effect of the heating rate on Weak Gel parameters

$$G = s \cdot (Hs) \cdot t^{-\alpha(H\alpha)}$$

Heating rate effect on stress  $Hs$

$$42^\circ\text{C} < T \leq 84^\circ\text{C} \text{ and } dT/dt > 1$$

$$Hs = (a_{2s} \cdot T + a_{3s}) \cdot \log\left(\frac{dT}{dt}\right) + 1$$

$84^{\circ}\text{C} < T \leq 110^{\circ}\text{C}$  and  $dT/dt > 1$

$$H_s = (-0.1962) \cdot \log\left(\frac{dT}{dt}\right) + 1$$

$T > 110^{\circ}\text{C}$

$$H_s = 1$$

$$a_{2s} = -0.0025$$

$$a_{3s} = 0.0177$$

Heating rate effect on the power index  $H\alpha$

$42^{\circ}\text{C} < T \leq 110^{\circ}\text{C}$  and  $dT/dt > 1$

$$H\alpha = (a_{1n} \cdot T + a_{2n}) \cdot \log\left(\frac{dT}{dt}\right) + 1$$

$T > 110^{\circ}\text{C}$

$$H\alpha = 1$$

$$\alpha_{1\alpha} = 0.0057$$

$$\alpha_{2\alpha} = -0.2181$$

**Rupture work from Bi-axial extension measurements**

$$W_{rupt} = 64000 \text{ Watt/m}$$

**Elastic recovery from creep measurements**

**Flour 1:**

$$J_0 = 0.593$$

$$J_1 = 0.139$$

$$J_2 = 0.133$$

$$J_3 = 0.133$$

$$\tau_1 = 3.833$$

$$\tau_2 = 58.1$$

$$\tau_3 = 395.202$$

**Flour 2:**

$$J_0 = 0.5693$$

$$J_1 = 0.1531$$

$$J_2 = 0.1327$$

$$J_3 = 0.1446$$

$$\tau_1 = 3.783$$

$$\tau_2 = 58.92$$

$$\tau_3 = 402.5133$$

The data for the memory are obtained through the following equation:

$$t^* = t_c - (A \cdot t_c + B) \cdot (1 + a \cdot \varepsilon^3)^{1/2}$$

Flour1:

$$A = 0.1778$$

$$B = 5.4734$$

$$a = 7805.6$$

Flour2:

$$A = 0.1659$$

$$B = 5.2781$$

$$a = 7805.6$$

**Heat and Mass transport coefficients.**

**Heat transport coefficient**

$$h_{ext} = 5 \text{ [W/m}^2\text{]}$$

**Mass transport coefficient**

Water in air [mole/(s·m<sup>2</sup>)]:

$$K_{yW} = \frac{h_{ext} \cdot 1000}{MW_{Air} \cdot C_{PAir}} \cdot \left( \frac{C_{PAir} \cdot P_{atm} \cdot MW_{Air} \cdot D_{W/A}}{101325 \cdot 0.0821 \cdot T \cdot K_{Air}} \right)^{2/3}$$

Ammonia in air [mole/(s·m<sup>2</sup>)]:

$$K_{yNH_3} = \frac{h_{ext} \cdot 1000}{MW_{Air} \cdot C_{PAir}} \cdot \left( \frac{C_{PAir} \cdot P_{atm} \cdot MW_{Air} \cdot D_{NH_3/A}}{101325 \cdot 0.0821 \cdot T \cdot K_{Air}} \right)^{2/3}$$

Carbon Dioxide in air [mole/(s·m<sup>2</sup>)]:

$$K_{yCO_2} = \frac{h_{ext} \cdot 1000}{MW_{Air} \cdot C_{PAir}} \cdot \left( \frac{C_{PAir} \cdot P_{atm} \cdot MW_{Air} \cdot D_{CO_2/Air}}{101325 \cdot 0.0821 \cdot T \cdot K_{Air}} \right)^{2/3}$$